

# 18th WEDC Conference

## KATHMANDU, Nepal 1992



## WATER, ENVIRONMENT AND MANAGEMENT

## Plastic media for waste water treatment

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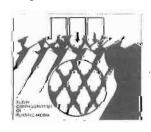


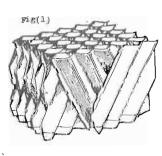
#### INTRODUCTION

design a Engineers always treatment plant to accomplish a particular degree of treatment, but a complete or 100% removal of the pollutant is uneconomical and never aimed at. Distilleries, paper and pulp, to name a few, discharge high strength biological effluents; treatment of the biological waste has to be carried out for cost efficient and for low recurring cost. Fixed film plastic media in the form of modular sheets has been extensively used for aerobic and anaerobic processes and the plastic media in the form of hexagonal tubes has been used for sedimentation process. This paper deals with the salient features performance of these plastic media waste water treatment.

#### FEATURES OF MODULAR MEDIA

Basically there are two types of plastic media - random and modular. Modular media is again of two types - straight lateral and cross flow. This paper deals with the cross flow type. The plastic material would be of PVC and thermoformed to form sheets having triangular wave like flutes. Each sheet is corrugated at 60° and is glued to the next sheet to form a particular criss cross pattern (fig 1). There are nearly 4000 contact





points per cu.m. of module and this provides internal mixing & redistribution which increases the liquid film diffusion of the waste water across the biomass. Around 95% voidage is there in the module for free access of air and has a specific surface area of 100 - 240 sq.m / cu.m.

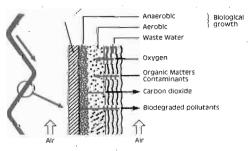
## FEATURES OF TUBULAR MEDIA

The plastic media in the form of tubes are a form of parallel plate gravity seperators and are called as Tubesettlers. These tubesettlers are manufactured from PVC, that follows the formation configuration. tubes in various The tubes are hexagonal in cross section and has a perimeter of 50 cms. The tubesettler has a specific surface area of 11 sq.m / cu.m and are inclined at 60°. The individual tubes are joined together to form a bundle of tubes.

#### APPLICATIONS

## Bio Filter Treatment

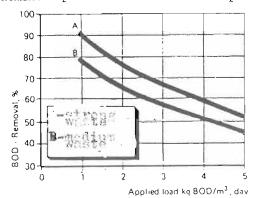
Trickling filter or bio filter is a reliable system for reducing high and medium strength BOD<sub>5</sub> in the waste water. The waste water is spread over the plastic media in the bio filter. On the media a bio film is growing and builds up by itself. The process of conversion is explained in fig 2. The voidage of the media gives enough room for developing the bio film without bridging one sheet to the other

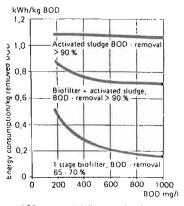


without disturbing the air flow. Modified VELZ equation has been considerede to be the best mathematical modelling for the optimum design of high rate bio filter with plastic media.

$$Ln(S_i / S_o) = \frac{K_{20} \times A_s \times D \times Y}{Q^n}$$

where  $S_1$ ,  $S_2$  are inlet and outlet BOD, in ppm,  $K_2$  the rate constant,  $A_2$  specific surface area in sq.m / cu.m,  $D_2$  the depth of the media in M,Y the temperature coeffecient,  $T_2$  the operating temperature in °C,  $Q_2$  the feed flux in cu.m/ sq.m./hr,  $T_2$  the constant. Experimentally, it has been determined the value of  $T_2$  to be .0024 for  $T_2$  of 100. Often it has been found, that it is more economical to use bio filters in the roughing stage, wherein  $T_2$  is reduced by  $T_2$  of  $T_2$  and suspended solids to above  $T_2$  and suspended solids to above  $T_2$  and conditions for the design of bio filters using plastic media and  $T_2$  gives the relative energy consumption of various treatment options. Bio filters provide





BOD - content in influent to biological stage

an effective means of oxidising ammoniacal nitrogen to nitrite nitrogen of secondary treated waste water. To treat a paper mill effluent having a flow of 14100cu.m/d,  $BOD_5$  of 650ppm, plastic media volume was around 6300 cu.m to reduce the  $BOD_5$  to 20ppm by 2 stage bio filter. Following table gives the performance of bio filters, where the flow is in NGD,  $BOD_5$  in ppm, and the media volume in cu.ft.

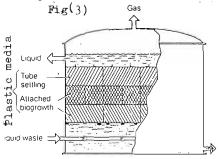
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Flow :	BOD <sub>5</sub> in	BOD's out	Media Volume	
++				•
0.6	210	10	119,300	
1.8	240	20	25,000	
2.3	127	10	31,400	
7.0	135	18	265,000	

### Revamping Bio Filters

The high performance of plastic media makes it an ideal way to upgrade the existing bio filter fitted with stone media. Revamping the existing bio filter with stone media by plastic media may be necessary due to a) non availablity of area to construct new filters, b) increase in applied, organic hydrolic loads, c) demand for better effluent standards and d) detoriation of the stone media. For each of the above conditions, replacement by plastic media is economical and effecient. It is possible to increase the height of the existing bio filter to 6 M high without changing the supporting and distributing system, to achieve desired effeciency. Upgrading rock media with plastic media has reported high results at waste water treatment plant at Seneca army depot, New York, Florida waste water treatment plant, Bridgeport Pennsylvania waste treatment plant and others.

## Anaerobic treatment

Plastic modular media in the anaerobic offer a greater digesters to the attached growth, while enhancing the tube settling action to retain the solids in the reactor and the growth of the active bio mass in the reactor. The surface within the media is specially designed that a controlled flow distributi -on is achieved, which is essential to ensure an intense contact between the biomass and the waste water. At a nominal film thickness of 3mm, about 300 Kgs of anaerobic sludge per cu.m will be available as an attached growth totally unaffected by the hydraulic fluctuations. A rough schematic shown in fig 3.



Following table gives the plastic media volume for various duty conditions when used in the anaerobic digestors.

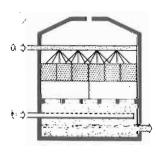
S1#	Flow	$BOD_5$ in	COD	in	Media	vol Source
1 2 3 4	125 225 200 420	50000 40000 2500 1400	1000	000 000 500 L00	850 2000 40 75	distillery distillery fruit pulp dairy

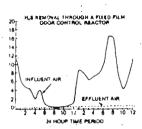
Flow in cu.m/d,  $BOD_5$ , COD in ppm, and media volume in cu.m.

Reduction of 90% BOD, were achieved in all the above cases. Sl# 1 & 2 are for biogas generation. The gas yeild was noticed at 0.3 NM / Kg of COD destroyed. The main constituent of the gas was methane with 65%. There are reports of anaerobic processes operating at a specific loading of 27 Kg COD/d/cu.m. Bacardi process developed by Larsen of U.S. are the pioneers in using plastic media for use in anaerobic digestors to treat cane sugar based mollasses distillery effluent.

## Odour Scrubbing

Objectionable odour in the form of Hydrogen Sulphide generated from waste water treatment facilities can be effectively oxidised with plastic media having specific surface area of 240M/M In a scrubber, similar to that of a scrubber in a degassification plant. The air containing the abnoxious compound is biologically oxidised by the biomass sustained on the plastic media. This oxidation occurs as the treated wastewater is applied across the top of the media counter to the upward flow of the air being treated. H2S removal to below 2ppm can be accomplished as shown in Graph 3. Other traditional methods calls for chemical storage, feed control and sludge generation which are totally eliminated in this scrubber (see fig 4).





a. Applied hydraulics b. Foul air from filter/other

### Sedimentation

The conventional mechanical clarrifier operate at an overflow rate of 1-2 cu.m/sq.m/Hr, while these hexagonal tube settlers operate at 7-9 cu.m/sq.m/hr, making it atleast 3 times more effecient. The criteria for designing the tube settler are the settling velocity, particle size and the sludge volume index of the suspended matter. tube settlers has a specific weight of 65 Kg/cu.m and can be housed with simple supports. These tube settlers can also be used in conjunction with the existing clarrifier mechanism and while doing so they increase the effeciency of the system. It is also possible to use the tube settler as a total replacement of the existing clarrifier. Advantages of tube settler include a) reduced size of clarrifier, means reduction in initial investment, b) no power requirement and c) no moving parts which means nil recurring cost. Care should be taken to size the tube settler for clarrification. Normally, tube settlers are of 0.5 - 1 metre in vertical height. Among the other geometry available, it is found that hexagonal tube settlers are more efficient.

### CONCLUSIONS

Plastic media being inert to most chemical and biological can be effectively used in the bio filters, anaerobic digestors and in the clarrifier systems. The normal practice is to use PVC, but the latest trend is shifting towards PP material, due to its ability to withstand higher operating temperatures when handling high to medium strength biological waste water and medium to low suspended solids, plastic media are an effective and economical alternative.

### REFERENCES

C.K.TIWARI,1980 - Bacardi Anaerobic digestion for treatment of distillery spent wash - simposium on treatment options at IIT Bombay-December 89.

TYLER RICHARDS, DEBA REINHART-1986, Evaluation of plastic media in trickling filters-Journal water pollution control-774-782, July 86.

DENNIS K. WOOD- 1989, Evaluation shows plastiv media to be more effective than rock filters-John Carollo engineers.